AMENDMENTS TO THE CLAIMS

The following listing of claims will replace all prior versions and listings of claims in the application.

LISTING OF CLAIMS

1. (Currently Amended) A method for high temperature short-time distillation of a residual oil originating from the processing of crude petroleum, natural bitumen or oil sand,

wherein in a mixing apparatus (1) the residual oil is mixed with granular hot coke as heat transfer medium, converted into oil vapour, gas and coke, and

wherein the gas[[es]] and oil vapour[[s]] are evacuated from the mixing apparatus (1) while being substantially separated from the granular coke, and

wherein the gas[[es]] and the vapour[[s]] are cooled down to produce ~~and a product~~ oil in form of condensate as well as gas ~~is produced~~ , and

wherein the coke, which has been evacuated from the mixing apparatus (1), is heated again ~~heated~~ and returned into the mixing apparatus (1) as heat transfer medium,

characterized in that the oil vapour and the gas ~~vaporized product oil~~ is partially condensed in a column (17) at temperatures beneath 450° C while adding gas or water vapour to the column (17) for reducing ~~the~~ partial pressure, and

wherein a high-boiling fraction is extracted from ~~this~~ the column (17) and ~~the~~ non condensed gas[[es]] and oil vapour[[s]] are evacuated from the column (17).

2. (Currently Amended) A method according to claim 1, characterized in that the non condensed gas[[es]] and oil vapour[[s]] from said column (17) are introduced into a second fractionating column (19), in which the product oil, which has not been condensed in the first column (17), is decomposed into vacuum gas oil having a low content of pollutants as well as a benzine/gas oil fraction.

3. (Currently Amended) A method according to claim 1, characterized in that ~~self-produced, returned product~~ the gas ~~is~~ introduced ~~as gas~~ into said column (17) to reduce the partial pressure is the non condensed gas coming from the column (17).

4. (Currently Amended) A method according to claim 1, characterized in that the partial pressure of the product oil in column (17) is reduced to such an extend that at temperatures beneath 450° C a highly boiling fraction having an initial boiling point between 450° C and 650° C can be condensed and ~~be extracted separately~~ separated from the other product oil fractions.

5. (Currently Amended) A method according to claim [[1]]4, characterized in that the separated highly boiling fraction contains more than 60% of the Conradson carbon residue (CCR), which is still contained in the product oil vapour[[s]], more than 70% of the heavy metals nickel (Ni) and vanadium (V), which are still contained in the product oil vapour[[s]], as well as more than 80% of the asphaltenes, which are still contained in the product oil vapour[[s]].

6. (Currently Amended) A method according to claim 1, characterized in that the ~~gas/oil~~ gas and the oil vapour evacuated from ~~mixture from~~ the mixing apparatus (1) ~~is~~ are dedusted in a cyclone (14) before being introduced in said column (17).

7. (Currently Amended) A method according to claim 1, characterized in that said column (17) is a quench cooler with a downstream multi-venturi washer, in which the gas[[es]] and vapour[[s]] originating form the mixing apparatus (1) are cooled and residual breeze is washed out.

8. (Currently Amended) A method according to claim [[1]]4, characterized in that the high boiling fraction, which has been separated in said column (17), is returned into said mixing apparatus (1).